

## The Peclet Problem

The convection-diffusion equation

$$\begin{aligned}
 \mathcal{L}(T) &= \frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} - \frac{\partial}{\partial x} \left( \frac{k}{\rho c_p} \frac{\partial T}{\partial x} \right) - \frac{s}{\rho c_p} = 0 & \Omega \in (0, L) \\
 l(T(x_L, t)) &= k \frac{\partial T}{\partial x} + h(T - T_r) = 0 & \partial\Omega_1 \in 0 \\
 T(x_R, t) &= T_R & \partial\Omega_2 \in L \\
 T(x, t_o) &= T_o(x) & \Omega, \partial\Omega
 \end{aligned} \tag{1}$$

can be further explored upon non-dimensionalization. Letting a superscript asterisk denote a non-dimensional variable, the non-dimensionalization of (1) involves the following definitions:

$$\begin{aligned}
 x^* &= \frac{1}{L} x & k^* &= \frac{1}{k_{ref}} k \\
 t^* &= \frac{U}{L} t & \rho^* &= \frac{1}{\rho_{ref}} \rho \\
 T^* &= \frac{T - T_{min}}{T_{max} - T_{min}} & c_p^* &= \frac{1}{c_{p,ref}} c_p \\
 u^* &= \frac{1}{U} u & h^* &= \frac{L}{k_{ref}} h \equiv Nu \\
 s^* &= \frac{L}{U(T_{max} - T_{min})\rho_{ref}c_{p,ref}} s
 \end{aligned} \tag{2}$$

Substituting the above definitions along with the non-d groups  $Re = \rho_{ref}UL/\mu_{ref}$ ,  $Pr = \mu_{ref}c_{p,ref}/k_{ref}$ , and  $Pe = Re Pr$  and doing a bit of tedious algebra results in:

$$\begin{aligned}
 \mathcal{L}(T^*) &= \frac{\partial T^*}{\partial t^*} + u^* \frac{\partial T^*}{\partial x^*} - \frac{1}{Pe} \frac{k^*}{\rho^* c_p^*} \frac{\partial}{\partial x^*} \left( \frac{\partial T^*}{\partial x^*} \right) - \frac{s^*}{\rho^* c_p^*} = 0 & on \Omega \\
 l(T^*(x^* = 0, t^*)) &= k^* \frac{\partial T^*}{\partial x^*} + Nu(T^* - T_r^*) = 0 & on \partial\Omega_1 \\
 T^*(x^* = 1, t^*) &= T_R^* & on \partial\Omega_2 \\
 T^*(x_o^*, t_o^*) &= T_o^*(x^*) & on \Omega, \partial\Omega
 \end{aligned} \tag{3}$$

For constant dimensional values of  $u = U$  (convection velocity),  $k = k_{ref}$  (thermal conductivity),  $\rho = \rho_{ref}$  (density), and  $c_p = c_{p,ref}$  (specific heat), the non-dimensional values become  $u^* = k^* = \rho^* = c_p^* = 1$ . For simplification, we shall assume there to be no source term, hence  $s^* = 0$ . Finally, we impose pure Dirichlet boundary conditions of  $T_{min}^*$  and  $T_{max}^*$  on  $\partial\Omega_1$  and  $\partial\Omega_2$  respectively, hence

$$\begin{aligned}
 \mathcal{L}(q) &= \frac{\partial q}{\partial t} + \frac{\partial q}{\partial x} - \frac{1}{Pe} \frac{\partial^2 q}{\partial x^2} = 0 & on \Omega \\
 q(x = 0, t) &= 0 & on \partial\Omega_1 \\
 q(x = 1, t) &= 1 & on \partial\Omega_2 \\
 q(x, t_o) &= q_o(x) & on \Omega, \partial\Omega
 \end{aligned} \tag{4}$$

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where the asterisks have been dropped for convenience and  $T$  has been replaced with a generic  $q$ .

The above problem statement is termed *the Peclet problem* and is a standard verification problem in the FEA/CFD community as the *steady state solution* is

$$q(x) = \frac{1 - e^{Pe x}}{1 - e^{Pe}} \quad (5)$$

It is not uncommon to obtain steady state solutions by “guessing” an initial condition (which may not satisfy the governing PDE!) and then using  $\Theta = 1$  to move forward in time until steady state is achieved. Note that, for this problem, the steady state solution is independent of the imposed initial condition - this may not be true for other problem statements!

**Homework:** For the Peclet problem, verify the non-dimensionalization, obtain the GWS<sup>h</sup>,  $\Theta$ TS, and NIA. Identify the terms which go into {FQ} and [JAC] and their associated Matlab syntax. While we seek the steady state solution, include the transient term in your analysis.